

METHOD AND FEEDSTOCK FOR MAKING SILICA BY FLAME COMBUSTION

Background of Invention

Field of the Invention

The invention relates generally to methods and feedstock for making silica.

Background Art

5 Silica is a particularly suitable material for forming the core and cladding of an optical waveguide. For the core of the optical waveguide, silica may be doped with a small amount of other dopant materials, such as titanium oxide, tin oxide, phosphorous oxide, aluminum oxide, and germanium oxide, to slightly increase the refractive index of the core above that of the cladding. In other fibers the core is pure silica and the
10 cladding is down doped with fluorine. Optical waveguides exhibiting very low losses are generally formed by vapor deposition processes. In one such process, a silica precursor is introduced into a conversion flame to produce fine particles, called "soot." A dopant material, such as GeCl_4 , may also be introduced into the conversion flame along with the silica precursor (*e.g.*, SiCl_4). The soot is deposited on an outside surface
15 of a rotating mandrel to form a soot preform. After an appropriate diameter of the core of the waveguide is reached, the mandrel is removed from the soot preform, leaving a hole in the soot preform. The soot preform is then sintered to form a consolidated glass draw preform. Next, the preform is drawn to close the hole and stretch the preform into a core cane of constant diameter. The core cane is then cut into segments, each of

which becomes a deposition surface for cladding. The core cane is overlaid with silica soot to an appropriate diameter and again consolidated. The resulting preform is then drawn until an optical waveguide having the desired dimensions is formed. For multi-segment fiber profiles, such as W profiles or ringed profiles, this process may include several steps of deposition, consolidation, and core-cane formation, with the dopants being provided to accomplish the desired refractive index for each segment.

Silica has also found a variety of uses in applications requiring transmission of ultraviolet radiation, particularly at wavelengths below 300 nm. One such application is in microlithography systems, which are employed in the production of integrated circuits. These systems use multiple fused silica lenses, called stepper lenses, to transmit radiation from excimer lasers to photosensitized silicon wafers. Current microlithography systems use 248-nm radiation (KrF laser) or 193-nm radiation (ArF laser) to print patterns with width as small as 0.25 μm . More advanced microlithography systems using 157-nm radiation (F_2 laser) are actively under development and are expected to produce patterns with even smaller widths. Microlithography systems require lenses made from high-purity fused silica because impurities in the lenses can distort the images projected onto the wafers as well as decrease transmission of the lenses. High-purity fused silica is typically produced by the boule process. The conventional boule process involves passing a silica precursor into a flame of a burner to convert the silica precursor to soot. The soot is then directed downwardly to a bait and immediately consolidated into dense, transparent, bulk glass, commonly called a boule. The boule can be used individually to fabricate stepper lenses as well as other optical elements such as photomasks.

It has been found that the selection of the silica precursor used in the production of silica is as important as the design of the equipment used to produce the silica. For a long time, the standard feedstock used in the production of silica was SiCl_4 . SiCl_4 was chosen because it yielded large amounts of vapors at low temperatures. Flame combustion of SiCl_4 , however, has a drawback because it produces chlorine gas as a by-product. If the conversion flame is provided by combustion of a hydrogen-containing fuel, which is usually the case, hydrogen chloride gas is also produced as a by-product. Moreover, large amounts of water (H_2 , OH, and H_2O) are formed. These gases are environmentally unfriendly and require considerable care for their disposal.

In addition, chlorine has been found to decrease transmission at 157 nm. This makes chlorine-based silica precursors unsuitable for making, for example, fused silica lenses for 157 nm applications.

Hydrogen-containing organic compounds such as octamethyltetrasiloxane and silane have been identified as satisfactory chlorine-free precursors for producing silica. However, flame combustion of these precursors also inherently result in the silica containing residual water, *i.e.*, OH, H₂, and H₂O. In optical waveguides and 157-nm applications it is preferable that the silica is substantially free of residual water. For optical waveguides, residual water in the silica results in high transmission loss in the optical waveguide. In preparation of fluorine-doped soot preform for optical waveguides, residual water is detrimental because it promotes fluorine migration. Water is known to reduce transmission of fused silica at wavelengths below 185 nm. Therefore, there is a strong interest in a method of producing silica that is substantially free of water and chlorine.

Summary of Invention

In one embodiment, the invention relates to a method for making silica which comprises delivering a silica precursor comprising a perfluorinated group to a conversion site and passing the silica precursor through a flame to produce silica soot. The perfluorinated group preferably comprises a group selected from the group consisting of alkyl, alkenyl, alkoxy, and aryl.

In another embodiment, the invention relates to a method for making silica which comprises a silica precursor comprising a chloro-derivative or fluoro-derivative or both to a conversion site and passing the silica precursor through a flame to produce silica soot.

Other features and advantages of the invention will be apparent from the following description and the appended claims.

Brief Description of Drawings

Figure 1A is a schematic representation of an OVD process for producing an optical waveguide preform.

Figure 1B is a schematic of a soot preform.

Figure 2 illustrates a process for producing doped silica soot.

Figure 3 is a schematic representation of a boule process for producing fused silica.

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Detailed Description

Embodiments of the invention use silicon compounds containing a perfluorinated group as replacements for the chloride-based and hydrogen-containing organic feedstock that are oxidized by flame hydrolysis to produce silica. The silicon compounds containing a perfluorinated group have the advantage of being oxidized without inclusion of water or chlorine in the silica. In general, the silicon compound may be any perfluorinated alkoxy-, alkyl-, alkenyl-, or aryl-silane. Representative formulae of these silicon compounds include, but are not limited to, $\text{Si}(\text{OR}_\text{F})_x\text{F}_{4-x}$ and $\text{Si}(\text{R}_\text{F})_x\text{F}_{4-x}$, where R_F is any perfluorinated alkyl, alkoxy, alkenyl, or aryl group and x is an integer ranging from 1 to 4.

In applications, such as fiber applications, where chlorine level in the silica is not of concern, the silicon compounds containing a perfluorinated group may also contain chlorine and/or fluorine as substituents. A representative formula of these silicon compounds is $\text{SiCl}_x\text{F}_y(\text{R}_\text{F})_z$, where x , y , and z are integers, the sum of x , y , and z is 4, and R_F is any perfluorinated alkyl, alkoxy, alkenyl, or aryl group.

In other embodiments where chlorine level in the silica is not of concern, silicon compounds containing chloro derivatives, fluoro derivatives, or chloro-fluoro derivatives may be used as a precursor in making the silica. Representative formulae of these types of silicon compounds include, but are not limited to, $\text{Si}(\text{R}_\text{F})_4$ and $\text{Si}(\text{OR}_\text{F})_4$, where R_F is CF_3 , CClF_2 , CCl_2F , CCl_3 , C_2F_5 , and so forth.

Various embodiments of the invention will now be described with reference to the accompanying drawings. Figure 1A is an exemplary schematic representation of an outside vapor deposition (OVD) process for producing an optical waveguide preform according to an embodiment of the invention. The process for producing the optical waveguide preform includes delivering a silica precursor 2 to a conversion site 4. The silica precursor 2 may be any of the silicon compounds described above. Preferably,

the conversion site 4 includes at least one burner 6 which produces a conversion flame 8. The burner 6 produces the conversion flame 8 by burning a fuel 14 and oxygen 16. The fuel 14 and oxygen 16 may be separately delivered to the burner 6 through fume lines 17 and 19, respectively. Mass flow controllers 21 and 23 are provided to control the rate at which fuel 14 and oxygen 16 are delivered to the burner 6. Alternatively, the fuel 14 and oxygen 16 may be mixed together in a premixing chamber (not shown). The fuel/oxygen mixture can then be delivered to the burner 6.

The oxygen 16 supplied to the burner 6 may be in its pure state or may be admixed with inert gases such as nitrogen, argon, helium, carbon dioxide, or chlorine. To provide a hydrogen-free environment for the OVD process, the fuel 14 preferably does not contain hydrogen or water. A suitable fuel for this purpose is carbon monoxide. To use carbon monoxide, a precursor which burns exothermically is desired because of the somewhat lower flame temperature as compared to, for example, CH_4 . Other examples of fuels include, but are not limited, to those containing $(\text{CN})_2$, $(\text{CNO})_2$, or a mixture of these gases. The fuel 14 may also be CO mixed with $(\text{CN})_2$, $(\text{CNO})_2$, D_2 or a mixture of these gases.

In one embodiment, the silica precursor 2 is delivered to the burner 6 in vapor form. If the silica precursor 2 does not exist in vapor form at room temperature, a liquid feedstock of the silica precursor 2 may be vaporized in a container 5, which may be a vaporizer, bubbler, or other similar equipment for vaporizing the feedstock. In this case, an inert carrier gas 10 is passed through the generated vapors to entrain the vapors and carry them to the burner 6 through a tubing 12. The inert carrier gas 10 could be any nonflammable gas such as nitrogen, noble gases (e.g., argon, helium, neon, krypton, xenon), nitrogen oxide, or fluorinated gases. Typical fluorinated gases are CF_4 , chlorofluorocarbons, e.g., $\text{CF}_x\text{Cl}_{4-x}$, where x is an integer ranging from 1 to 3, NF_3 , SF_6 , SiF_4 , C_2F_6 , and SF_6 . It should be noted that chlorofluorocarbons should be avoided if a chlorine-free process is desired. While transporting the silica precursor vapors to the burner 6, the tubing 12 may be heated to prevent condensation of the vapors. Also, another stream of inert gas (not shown), e.g., nitrogen, may be brought in contact with the silica precursor vapors to prevent saturation of the vapors. A mass flow controller 13 may be used to control the rate at which the vapors are delivered to the burner 6.

At the conversion site **4**, the silica precursor vapors pass through the conversion flame **8** to form soot **18**, which is deposited on a mandrel **20**. Typically, the mandrel **20** is a tapered cylindrical member made of an inert material such as alumina. A glass handle **24** is provided over the mandrel **20** at one end and is used for gripping the soot preform **22** throughout the process. A spacer **25** holds the handle **24** relative to the mandrel **20** prior to depositing the soot **18** on the mandrel **20**. To allow for uniform deposition, the mandrel **20** is rotated and translated axially as layers of the soot **18** are deposited. To maintain the hydrogen- and water-free environment, the conversion site **4** and mandrel **20** should be enclosed in an atmosphere that is free of moisture and hydrogen gas, such as dry air or dry inert gas (e.g., argon, krypton, helium, neon, xenon, or nitrogen), as depicted by the dotted box **3** around the preform **22** and flame **8**.

The soot **18** is deposited on the mandrel **20** until the appropriate diameter of the optical waveguide core, or soot preform **22**, is formed. After deposition, the mandrel **20** is removed from the soot preform **22**. Referring to Figure 1B, removal of the mandrel (**20** in Figure 1A) leaves a hole **27** extending along an axial length of the soot preform **22**. A plug-like member **29** made of pure silica is inserted at one end of the hole **27**, i.e., the end that does not include the glass handle **24**. The plug-like member **29** will close that end of the preform upon consolidation. The soot preform **22** is inserted into and held in a consolidation furnace (not shown) and fully consolidated. It should be noted that when the soot preform **22** is produced in a hydrogen- and water-free environment, a chlorine treatment to remove residual water may not be necessary before full consolidation. In this case, the soot preform **22** is also preferably transported to the consolidation furnace (not shown) in a substantially water-free environment.

The consolidated preform is drawn to close the hole **27** and stretched into core cane using conventional fiber draw techniques. The core cane is then cut into segments, each of which becomes a deposition surface for a silica overclad or further segments of the core, preferably including a fluorine dopant. The silica overclad or additional segments may be formed using the OVD process described above, except that the mandrel **20** will now be replaced with the core cane segment. The overclad core cane segment is finally consolidated and drawn into an optical waveguide. In the case where the cladding is F-doped, the dopant may be added during deposition or,

more preferably, during consolidation as is described in U.S. Patent No. 4,629,485 issued to Berkey. For multi-segment fiber profiles, such as W profiles and ring profiles, the process of forming the optical waveguide may include several steps of soot deposition, consolidation, and core cane formation. For example, the overlaid core

5 core segment can be drawn using conventional fiber draw techniques, cut into segments, and then used as a deposition substrate for the next segment.

The soot **18** may be doped with materials, such as F, B, Al, Ge, Sn, Ti, P, Se, Er, S, Ca, Ba, Y, Yb, Ta, La, Sb, and Bi, during the OVD process or consolidation to create different index profiles. Typical fiber compositions include germania (GeO_2) in the core to provide a higher index than the clad. Figure 2 illustrates a process for

10 producing doped silica soot in deposition. The process is similar to the one described in Figure 1A, except that an additional delivery system is needed for delivering the dopant material **26** to the burner **6**. In the illustration, the silica precursor **2** and the dopant material **26** are separately delivered to the burner **6** through lines **12** and **31**, respectively. Mass flow controllers **13**, **33** are provided to control the rate at which the

15 vaporous reactants **2**, **26** are delivered to the burner **6**. In an alternate embodiment, the silica precursor **2** may be mixed with the dopant material **26** prior to being delivered to the burner **6**. Preferably, the dopant material **26** is a gaseous material or vaporizable material.

To maintain the hydrogen-free environment, the dopant material **26** is preferably free of hydrogen. Similarly, to maintain a chlorine-free environment, the dopant material **26** is preferably free of chlorine. U.S. Application Serial no. _____, entitled "Method and Feedstock for Making Silica," filed _____, in the name of David L. Tennent and J. Marc Whalen, discloses a chlorine-free germania dopant which

20 comprises a pseudohalogen, *e.g.*, $\text{Ge}(\text{NCO})_4$.

Figure 3 is an exemplary schematic representation of a boule process for producing high purity fused silica using a silicon compound of the present invention. In the boule process, fuel **48** and oxygen **50** are mixed in a premixing chamber **52**. The fuel/oxygen mixture is then transferred to burners **56** mounted at the crown of a furnace

30 **57**. To maintain a hydrogen-free atmosphere, the fuel **48** is preferably hydrogen-free. As previously mentioned, a suitable fuel for this purpose is carbon monoxide. The burners **56** ignite the fuel/oxygen mixture to produce flames **60**, which typically preheat

the deposition cavity 62 to a desired temperature. Although only two burners 56 are shown, more burners may be used to achieve uniform heat distribution across the deposition cavity 62. A silica precursor 64 is delivered in vapor form to a distribution system 54, which distributes the vapors to the burners 56. The silica precursor 64 may be any of the previously described silicon compounds. If the silica precursor 64 does not exist in vapor form at room temperature, a liquid feedstock of the silica precursor 64 may be vaporized in a container 66 and an inert carrier gas 61 may be used to transport the vapors to the distribution system 54. As also shown in the figure, an inert gas 63 may be brought in contact with the precursor vapors to prevent saturation.

The silica precursor 64 vapors pass through the flames 60 and are converted to soot 67. The soot 67 is deposited on a substrate 68 (typically made of silica) and immediately consolidated into dense glass 70. Consolidation typically occurs at roughly 1550°C or greater. To ensure homogeneity, the substrate 68 is typically rotated and oscillated as the silica soot is deposited. Spurious soot formed during soot deposition is removed via draft ports 74 which are connected to an exhaust system (not shown). The furnace 57 is drafted using a purge gas 76. Preferably, the purge gas 76 is an inert gas, such as nitrogen, so that a substantially hydrogen-free environment is maintained. Generally, it is desirable to provide a pressurized atmosphere in the deposition cavity 62 greater than an atmospheric pressure outside of the deposition cavity 62.

Those skilled in the art will appreciate that various modifications to the embodiments described above are possible which are within the scope of the invention. For example, for the boule process, a dopant material, such as a hydrogen- and chlorine-free titania precursor, may be passed through the conversion flame along with the silica precursor to produce doped silica soot. The silica precursor of the present invention may also be used in other vapor deposition processes such as vapor-axial deposition process, wherein a column of soot preform is grown. In general, the invention can be used where the soot deposition and consolidation occur separately or simultaneously.

The invention described herein can make soot preforms or glass boules that are substantially free of hydrogen and chlorine. As previously discussed, such soot

preforms and glass boules are useful in many applications, such as optical waveguide fabrication and lens and photomask fabrication.

While the invention has been described with respect to a limited number of embodiments, those skilled in the art, having benefit of this disclosure, will appreciate that other embodiments can be devised which do not depart from the scope of the invention as disclosed herein. Accordingly, the scope of the invention should be limited only by the attached claims.